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President
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**Content Based
Chemical Engineering**

Summary

Piping Pressure Drop Template -- For Liquids or Gases
Version 2.19a

by Stephen M. Hall, PE
Copyright 1999, 2000

All cells are locked except user-defined data; unlock sheet from Tools menu (no password required)
VIEW-COMMENTS to see some additional explanations.

DATA INPUT			
Project Data			
Prepared by	S. Hall	Client	Sample
Date	15-Mar-2003	W.O.	10314
<input type="radio"/> English <input checked="" type="radio"/> SI		Unit	Process
		Area	Tank Farm
Line ID			
Line Number:	Liquid Example		
General Pipeline Data			
Service:	Raw Material Transfer		
Pipe Material Specification:	A	<< 150 lb Carbon Steel	
Insulation	None		
Ambient Temp (deg F)	80.00		
Process Data			
Fluid Name	Toluene	<input checked="" type="radio"/> Liquid <input type="radio"/> Gas	
Molecular Weight (Entry Ignored>>>)	92.13		
Actual Flow (gallons/minute)	100.00		
Maximum Flow (gallons/minute)	100.00		
Flowing Temperature (deg F)	70.00		
Nominal Pressure (psia)	14.70		
Specific Gravity	0.87 (<<< Entry Ignored)		
Absolute Viscosity (centipoise)	0.779 (<<< Entry Ignored)		
Size Selection Criteria			
<input type="radio"/> Economic <input checked="" type="radio"/> Specific Diameter <input type="radio"/> Target Velocity			
3			
Physical Layout			
Length of pipeline (feet)	1000		
90 deg Ell	0	Globe Valve	0
Long Rad. Ell	0	Gate Valve	0
45 deg Ell	0	Ball Valve (reduced p)	0
180 deg Bend	0	Butterfly Valve	0
TEE-Line Flow	0	Plug Valve	0
TEE-Branch Flow	0	Angle Valve	0
Bell Mouth Inlet	0	Swing Check Valve	0
Square Mouth Inlet	0	Re-Entrant Pipe	0
Report Selection			
<input checked="" type="checkbox"/> Results Summary	<input checked="" type="checkbox"/> LIQFLOW		
<input checked="" type="checkbox"/> Datasheet Style	<input checked="" type="checkbox"/> EquivLength		
<input checked="" type="checkbox"/> Instructions	<input checked="" type="checkbox"/> OPTLIO		

Optional Pulldown List of Fluids

Toluene

Conversion from scfm to pph

Desired scfm: 150

Molecular weight: 92.13

Actual Flow (lb/h): 2,310

Conversion from acfm to pph

Desired acfm: 150

Molecular weight: 92.13

Pressure (psia): 14.7

Temperature (deg F): 70

Actual Flow (lb/h): 2,144

				PIPELINE SIZING CALCULATION								
				CLIENT				LINE NO.				
				Sample				Liquid Example				
REV	PREPARED BY	DATE	APPROVAL	W.O.				REQUISITION NO.		SPECIFICATION NO.		
0	S. Hall	15-Mar-2003		10314						18103		
1				UNIT		AREA		PROCURED BY		INSTALLED BY		
2				Process	Tank Farm							
1	General											
2	Fluid Service			Raw Material Transfer								
3	Pipe Specification			A: 150 lb Carbon Steel								
4	Surface Roughness		(feet)	0.00015								
5	Insulation			None								
6	Ambient Temperature		(deg F)	80								
7												
8	Process Data											
9	Fluid Pumped			Toluene (liquid)								
10	Design Flow Rate		(gallons/minute)	100								
11	Maximum Flow Rate		(gallons/minute)	100								
12	Flowing Temperature		(deg F)	70								
13	Nominal Pressure		(psia)	14.7								
14	Specific Gravity			0.867 (= 54.10 lb/cu.ft.)								
15	Viscosity		(centipoise)	0.583587								
16												
17	Basis for Sizing: Optimum Economic Diameter											
18												
19		Nom.		O.D.	Wall	I.D.	Reynolds	Friction	Pressure Drop/100 equiv ft		Velocity	
20		Size	Sched	(in.)	(in.)	(in.)	Number	Factor	(psi)	(ft water)	(ft liq)	(ft/sec)
21		2	80	2.375	0.218	1.939	2.42E+05	0.0207	8.81	20.36	23.48	10.87
22	====>	3	40	3.500	0.216	3.068	1.53E+05	0.0199	0.85	1.97	2.27	4.34
23		4	40	4.500	0.237	4.026	1.17E+05	0.0198	0.22	0.51	0.58	2.52
24												
25	Physical Layout											
26	90 deg Ell	-	TEE-Line Flow	-	Globe Valve	-	Plug Valve	-				
27	Long Rad. Ell	-	TEE-Brnch Flow	-	Gate Valve	-	Angle Valve	-				
28	45 deg Ell	-	Bell Mouth Inlet	-	Ball Valve (red. port)	-	Swing Check Valve	-				
29	180 deg Bend	-	Sq. Mouth Inlet	-	Butterfly Valve	-	Re-Entrant Pipe	-				
30	Straight Feet of Pipe (measured through centerline of fittings):								1000 feet			
31												
32	Heat Loss											
33		Nom.						Pipe is Uninsulated				
34		Size		units			Bare	0.5 in	1 in	1-1/2 in	2 in	3 in
35		2		Btu/hr-ft			(7)	n/a	n/a	n/a	n/a	n/a
36	====>	3		Btu/hr-ft			(11)	n/a	n/a	n/a	n/a	n/a
37		4		Btu/hr-ft			(13)	n/a	n/a	n/a	n/a	n/a
38												
39	Summary of Results											
40		Nom.	Eq Lgth	Pressure Drop			Heat Loss (Gain), But/hr					
41		Size	(ft)	(psi)	(ft water)	(ft liq)	Bare	0.5 in	1 in	1-1/2 in	2 in	3 in
42		2	1,000	88.13	203.58	234.8	(7,363)	n/a	n/a	n/a	n/a	n/a
43	====>	3	1,000	8.54	19.73	22.7	(11,336)	n/a	n/a	n/a	n/a	n/a
44		4	1,000	2.19	5.06	5.8	(13,417)	n/a	n/a	n/a	n/a	n/a
45												
46												
47												
48												
49												
50												
51												
52												

				EFFECT OF FLOW VARIATION				
				CLIENT		LINE NO.		
				Sample		Liquid Example		
REV	PREPARED BY	DATE	APPROVAL	W. O.	REQUISITION NO.	SPECIFICATION NO		
0	S. Hall	15-Mar-2003		10314		18103		
1				UNIT	AREA	PROCURED BY	INSTALLED BY	
2				Process	Tank Farm			
1	General							
2	Fluid Service	Raw Material Transfer						
3	Pipe Specification	A: 150 lb Carbon Steel						
4	Surface Roughness (feet)	0.00015						
5	Insulation	None						
6	Ambient Temperature (deg F)	80						
7								
8	Process Data							
9	Fluid Pumped	Toluene (liquid)						
10	Design Flow Rate (gallons/minute)	100						
11	Maximum Flow Rate (gallons/minute)	100						
12	Flowing Temperature (deg F)	70						
13	Nominal Pressure (psia)	14.7						
14	Specific Gravity	0.867 (= 54.10 lb/cu.ft.)						
15	Viscosity (centipoise)	0.58359						
16								
17	Smaller Pipe Size	2 in.		Flow	Reynolds	Friction	DeltaP/100 equiv ft	Velocity
18	Schedule	80		(gpm)	Number	Factor	(psi) (ft water)	(ft/sec)
19	Outside Diameter (in.)	2.375		10	24,192	0.0270	0.11 0.26	1.09
20	Wall Thickness (in.)	0.218		20	48,384	0.0241	0.41 0.95	2.17
21	Inside Diameter (in.)	1.939		30	72,576	0.0229	0.87 2.02	3.26
22				40	96,768	0.0222	1.51 3.48	4.35
23				50	120,960	0.0217	2.31 5.33	5.43
24				60	145,152	0.0214	3.27 7.56	6.52
25				70	169,344	0.0211	4.40 10.17	7.61
26				80	193,536	0.0210	5.70 13.17	8.69
27				90	217,727	0.0208	7.16 16.54	9.78
28				100	241,919	0.0207	8.79 20.30	10.87
29	Selected Pipe Size	3 in.		Flow	Reynolds	Friction	DeltaP/100 equiv ft	Velocity
30	Schedule	40		(gpm)	Number	Factor	(psi) (ft water)	(ft/sec)
31	Outside Diameter (in.)	3.500		10	15,289	0.0289	0.01 0.03	0.43
32	Wall Thickness (in.)	0.216		20	30,579	0.0250	0.04 0.10	0.87
33	Inside Diameter (in.)	3.068		30	45,868	0.0233	0.09 0.21	1.30
34				40	61,158	0.0222	0.15 0.35	1.74
35				50	76,447	0.0215	0.23 0.53	2.17
36				60	91,737	0.0210	0.32 0.75	2.60
37				70	107,026	0.0206	0.43 1.00	3.04
38				80	122,316	0.0203	0.56 1.29	3.47
39				90	137,605	0.0201	0.70 1.61	3.91
40				100	152,895	0.0199	0.85 1.97	4.34
41	Next Larger Pipe Size	4 in.		Flow	Reynolds	Friction	DeltaP/100 equiv ft	Velocity
42	Schedule	40		(gpm)	Number	Factor	(psi) (ft water)	(ft/sec)
43	Outside Diameter (in.)	4.500		10	11,651	0.0306	0.00 0.01	0.25
44	Wall Thickness (in.)	0.237		20	23,303	0.0260	0.01 0.03	0.50
45	Inside Diameter (in.)	4.026		30	34,954	0.0240	0.02 0.05	0.76
46				40	46,605	0.0227	0.04 0.09	1.01
47				50	58,257	0.0219	0.06 0.14	1.26
48				60	69,908	0.0213	0.08 0.19	1.51
49				70	81,559	0.0208	0.11 0.26	1.76
50				80	93,210	0.0204	0.14 0.33	2.02
51				90	104,862	0.0201	0.18 0.41	2.27
52				100	116,513	0.0198	0.22 0.50	2.52

				SELECTED PIPE DIAMETER			
				CLIENT	LINE NO.		
				Sample	Liquid Example		
REV	PREPARED BY	DATE	APPROVAL	W. O.	REQUISITION NO.	SPECIFICATION NO.	
0	S. Hall	15-Mar-2003		10314		18103	
1				UNIT	AREA	PROCURED BY	INSTALLED BY
2				Process	Tank Farm		
1	General						
2	Fluid Service	Raw Material Transfer					
3	Pipe Specification	A: 150 lb Carbon Steel					
4	Surface Roughness (feet)	0.00015					
5	Insulation	None					
6	Ambient Temperature (deg F)	80					
7							
8	Process Data						
9	Fluid Pumped	Toluene (liquid)					
10	Design Flow Rate (gallons/minute)	100					
11	Maximum Flow Rate (gallons/minute)	100					
12	Flowing Temperature (deg F)	70					
13	Nominal Pressure (psia)	14.7					
14	Specific Gravity	0.867 (= 54.10 lb/cu.ft.)					
15	Viscosity (centipoise)	0.58359					
16							
17	Economic Data						
18	Purchase cost of new pipe, 1 inch diameter, \$/ft					\$1.75	
19	Ratio of costs for fittings & installation to purch. cost of pipe					5	
20	Factor relating pipe cost to diameter (exponential)					1.30	
21	Frictional loss due to fittings and bends, % of straight pipe					35%	
22	Operation, hours/yr					8,000	
23	Cost of electricity, \$/kwhr					\$0.15	
24	Efficiency of motor and pump, %					60%	
25	Annual fixed charges for maintenance, % of pipe cost					20%	
26							
27	Basis for Sizing: Optimum Economic Diameter						
28	Optimum diameter calculated using Peters & Timmerhaus formula					2.59	
29	Closest pipe size from specified material class					3	
30							
31		Smaller	Selected	Next Larger			
32		Size	Size	Size			
33	Actual Size	inch nominal size	2	3	4		
34		inch actual inside diame	1.939	3.068	4.026		
35	Velocity	feet/second	10.87	4.34	2.52		
36	Reynolds No.		241,919	152,895	116,513		
37	Friction Factor		0.0207	0.0199	0.0198		
38	Pressure Drop	psi/100 equiv ft	8.813	0.854	0.219		
39							
40	Calculated Costs, \$ per year per foot of installed piping:						
41			2	3	4		
42	Pumping Cost (power)		\$11.02	\$1.20	\$0.32		
43	Initial Piping (capital expenditure)		\$25.85	\$43.80	\$63.66		
44	Annual Piping (maintenance)		\$5.17	\$8.76	\$12.73		
45	Total		\$16.19	\$9.96	\$13.05		
46							
47							
48							
49							
50	Reference:	Peters & Timmerhaus					
51		Plant Design and Economics for Chemical Engineers					
52							
53							

Insulation Material Data

Table may be modified or supplemented. If adding new insulation material, insert new row prior to end of table (at row 15 for instance), add new materi

Insulation Material	Min. Thickness (in)	Thermal Conductivity Coefficients					Maximum Temperature (°F)	Minimum Temperature (°F)	Thermal Conductivity, K [Btu*in/(h*ft ² *°F)]
		<i>m</i>	<i>p</i>	<i>s</i>	<i>t</i>	<i>u</i>			
Calcium Silicate	1	0.369	1.58E-04	3.92E-07	9.40E-11	0.00E+00	1000	250	0.383
Cellular glass	1	0.289	5.14E-04	4.36E-07	2.27E-10	2.76E-13	900	-450	0.330
Elastometric foam	0.5						200	-40	0.290
Fiberglass	1	0.195	4.25E-04	0.00E+00	0.00E+00	0.00E+00	850	42	0.227
Mineral Wool	1	0.228	3.72E-04	6.00E-07	0.00E+00	0.00E+00	1200	42	0.259
Perlite, expanded	1	0.388	4.73E-04	3.06E-07	-8.00E-11	0.00E+00	1000	250	0.425
Phenolic foam	1	0.116667	6.67E-04				300	75	0.167
Polystyrene foam	1						165	-65	0.230
Polyurethane/ Polyisocyanurate foams	1	0.174	-1.55E-04	-3.39E-07	8.38E-09	1.82E-11	250	-200	0.165

Intermediate Calculations	
Wind Factor	0
2*pi*(Ti-Ts)	-62.83185307
K factor, per inch	0.02160625
Average temperature (fluid to ambient)	75 deg F

Insulation Material Data

Table may be modified or supplemented. If adding new insulation material, insert new row prior to end of table (at row 15 for instance), add new materi

Insulation Material	Min. Thickness (in)	Thermal Conductivity Coefficients					Maximum Temperature (°F)	Minimum Temperature (°F)	Thermal Conductivity, K [Btu*in/(h*ft ² *°F)]
		<i>m</i>	<i>p</i>	<i>s</i>	<i>t</i>	<i>u</i>			
Calcium Silicate	1	0.369	1.58E-04	3.92E-07	9.40E-11	0.00E+00	1000	250	0.383
Cellular glass	1	0.289	5.14E-04	4.36E-07	2.27E-10	2.76E-13	900	-450	0.330
Elastometric foam	0.5						200	-40	0.290
Fiberglass	1	0.195	4.25E-04	0.00E+00	0.00E+00	0.00E+00	850	42	0.227
Mineral Wool	1	0.228	3.72E-04	6.00E-07	0.00E+00	0.00E+00	1200	42	0.259
Perlite, expanded	1	0.388	4.73E-04	3.06E-07	-8.00E-11	0.00E+00	1000	250	0.425
Phenolic foam	1	0.116667	6.67E-04				300	75	0.167
Polystyrene foam	1						165	-65	0.230
Polyurethane/ Polyisocyanurate foams	1	0.174	-1.55E-04	-3.39E-07	8.38E-09	1.82E-11	250	-200	0.165

Intermediate Calculations	
Wind Factor	0
2*pi*(Ti-Ts)	-62.83185307
K factor, per inch	0.02160625
Average temperature (fluid to ambient)	75 deg F

Pipes

Standard Specifications										
Modify this table to incorporate project- or company-specific pipe specification designations. Keep it in alphabetical order by Spec.										
The column "Size Table" refers to the Pipe Specification Lookup Table section located below. Add additional columns if necessary, or edit the existing ones.										
Spec Code	Description	Min Temp deg F	Max Temp deg F	Max Press psig	Roughness ft	Cost Factors			Size Table	
						Purchase \$/ft (1 inch)	Ratio Fittings	Exponent		
A	150 lb Carbon Steel	-10	450	150	0.00015	\$1.75	5	1.3	2	
A3	125 lb Carbon Steel	-10	450	125	0.00015	\$1.75	5	1.3	2	
B	300 lb Carbon Steel	-20	750	300	0.00015	\$1.75	5	1.3	2	
C	316L SS Pipe	-100	500	145	0.0001	\$4.50	8	0.89	8	
CU	Copper Pipe	-100	250	110	0.000005	\$4.50	8	0.89	6	
D1	316L SS Sanitary Tubing	-100	450	150	0.000001	\$4.50	8	0.89	15	
D2	316L SS Zephyrweld Tubing	-100	450	150	0.000005	\$4.50	8	0.89	14	
F1	Teflon-Lined Pipe	-20	500	170	0.000005	\$4.50	8	0.89	9	
F2	PVDF-Lined Pipe, Heavy	-20	275	150	0.000005	\$4.50	8	0.89	10	
F3	PVDF-Lined Pipe, Thick	-20	275	150	0.000005	\$4.50	8	0.89	11	
F4	Polypropylene-Line Pipe	0	225	150	0.000005	\$4.50	8	0.89	12	
G	FRP Pipe, Epoxy Lining	0	225	150	0.000005	\$4.50	8	0.89	13	
GL	Glass-lined Steel	-20	450	150	0.000005	\$4.50	8	0.89	7	
H1	CPVC Pipe	0	180	100	0.000005	\$0.75	18	0.91	16	
H2	Polypropylene Pipe, SD	0	200	150	0.000005	\$4.50	8	0.89	17	
K	Type K Copper Water Tube	-100	250	110	0.000015	\$4.50	8	0.89	3	
L	Type L Copper Water Tube	-100	250	110	0.000015	\$4.50	8	0.89	4	
M	Type M Copper Water Tube	-100	250	110	0.000015	\$4.50	8	0.89	5	